

## Acidic and Catalytic Properties of Niobium Pentaoxide

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The surface acidic property of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  and its catalytic activities for the isomerization of 1-butene, the polymerization of propylene and the dehydration of 2-butanol were examined. The activities were high on  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  evacuated at moderate temperatures (100–150 °C) in all of the reactions and decreased drastically on evacuation at higher temperatures (400–500 °C). The surface of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  showed a strong acidic character ( $H_0 \leq -5.6$ ) even after heating in air at 100 °C, but the strong acid sites disappeared on heat treatment at higher temperatures. The active sites on the catalysts heat-treated at moderate temperatures were ascribed mainly to Brönsted acid sites on the basis of the IR study of adsorbed pyridine.

Although niobium oxides are reported in the patents to catalyze several reactions such as the oxidation of organic molecules,<sup>1)</sup> oxidative dehydrogenation of olefins or paraffins,<sup>2)</sup> and the decomposition of  $\text{NO}_x$ ,<sup>3)</sup> the details of surface property and catalytic activity are not known. On the other hand, catalysts containing molybdenum and vanadium, neighbors of niobium in the periodic table, are the most important industrial catalysts and their catalytic properties have been studied extensively by many workers. In this sense, it will be possible to use niobium oxides as a catalyst or an active component of catalysts for certain reaction. For this purpose, a fundamental knowledge about niobium oxides is required. Thus, we have studied the surface acid-base properties and the catalytic activities for the reactions of 1-butene, propylene, and 2-butanol as model reactions.

### Experimental

Niobium oxide was prepared by heating  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  (CBMM AD-108) in a vacuum or in air at various temperatures. The  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  was used after washing with distilled water followed by drying at 100 °C. The content of Nb in  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  was 55.54% and no impurity of K or Na was detected.

The differential thermal analysis (DTA) and thermogravimetry (TG) were done by using a Rigaku TG-DTA apparatus with the heating program rate of 10 °C/min. The X-ray diffraction pattern was taken by a Shimadzu XRD spectrometer with Cu  $K\alpha$  source. The surface area of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  was measured by using a conventional BET apparatus.

For the measurement of acidic and basic properties,  $\text{Nb}_2\text{O}_5$  was suspended in a benzene solution, basic or acidic indicators were adsorbed and the color change of indicators was observed.<sup>4)</sup> The indicators used were anthraquinone ( $pK_a = -8.2$ ), benzylideneacetophenone ( $-5.6$ ), dicinnamylideneacetone ( $-3.0$ ), Crystal Violet ( $+0.8$ ), 4-anilinoazobenzene ( $+1.5$ ), 4-dimethylaminoazobenzene ( $+3.3$ ), Methyl Red ( $+4.8$ ), and Bromthymol Blue ( $+7.1$ ).

Infrared spectra were recorded with a JASCO-701G spectrometer using an in situ cell. The sample was pressed into a thin wafer and placed in the cell. Pyridine was adsorbed on  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  which had been evacuated at various temperatures for 2 h and degassed at certain temperatures for 30 min. The IR spectra of adsorbed  $\text{CO}_2$  was also measured by the same method as in pyridine adsorption.

For the reactions of 1-butene and 2-butanol, a closed recirculation reactor having a volume of 300  $\text{cm}^3$  was used. After the evacuation of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  at various temperatures

for 2 h, 6.7 kPa of 1-butene or 1.4 kPa of 2-butanol was introduced at the reaction temperature. The polymerization activity of propylene was measured by observing the pressure decrease in a static reactor. The activity was obtained by measuring the rate of decrease in reactant pressure (initial pressure = 13.3 kPa) at 5 min reaction time to avoid the pressure decrease due to the adsorption in the initial stage of the reaction.

### Results

**X-Ray and Thermal Analysis of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$ .** The results of DTA and TG of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  are shown in Fig. 1(A). At around 90 and 180 °C, two endothermic peaks with the decrease of gravity were observed. These can be ascribed to the dehydration process of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$ . The dehydration was completed by heating up to 300 °C and the gravity change of the sample was not observed at 300–700 °C. The exothermic peak at

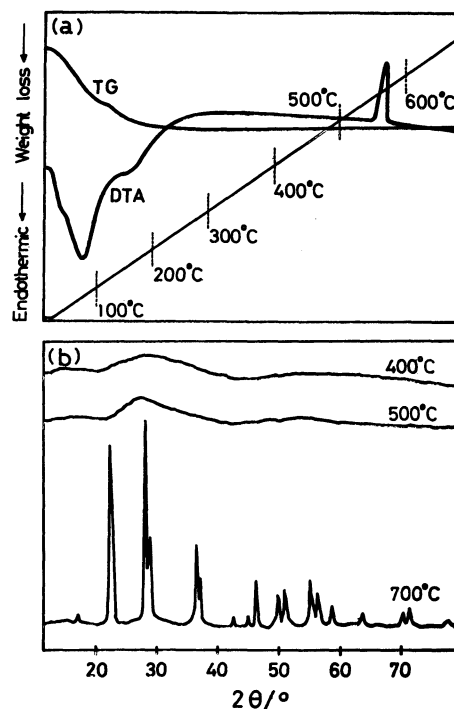


Fig. 1. (A) Thermogravimetry and differential thermal analysis of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$ . (B) X-Ray diffraction patterns of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  heat-treated at various temperatures in air.

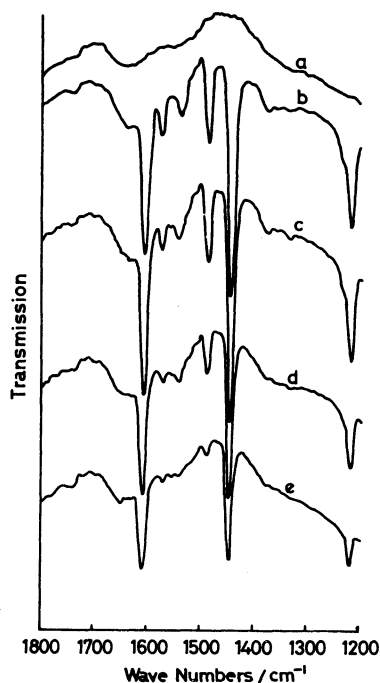


Fig. 2. IR spectra of pyridine adsorbed on  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$ . a: Background, b: degassed at room temperature after the adsorption, c: degassed at 100 °C, d: degassed at 200 °C, e: degassed at 300 °C.

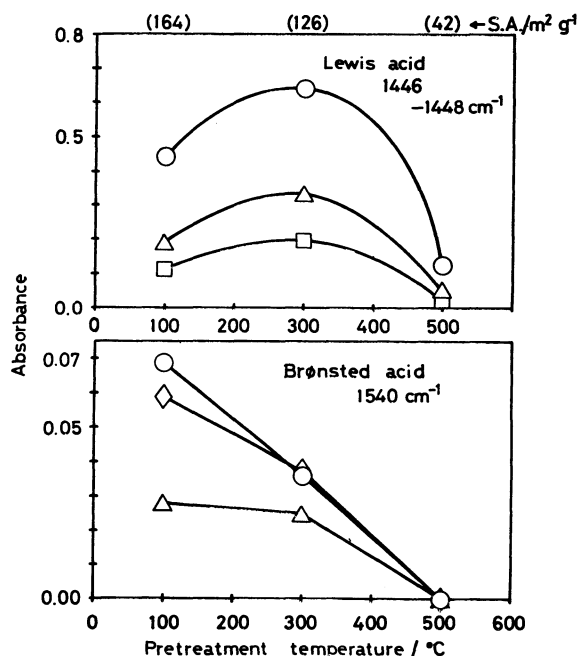


Fig. 3. Acidity change of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  with pretreatment temperature.

◇: Evacuated at room temperature after adsorption of pyridine, ○: at 100 °C, △: at 200 °C, □: at 300 °C.

about 550–570 °C with no gravity change might be due to a phase transformation.

X-Ray diffraction patterns of the samples which were heat-treated at different temperatures are shown in Fig. 1(B). After heating  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  at 400 °C in air, very broad peaks at  $2\theta \approx 30^\circ$  and around  $55^\circ$  were

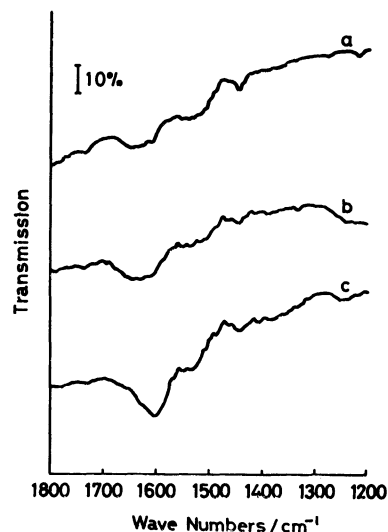


Fig. 4. IR spectra of  $\text{CO}_2$  adsorbed on  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  evacuated at 300 °C, a: background, b: evacuated at room temperature after the adsorption for 15 min, c: adsorption for 15 h.

observed. Upon heating at 500 °C in air, those peaks sharpened slightly. A good crystallinity was observed by heating at 700 °C and the diffraction pattern corresponded well to the T-T phase  $\text{Nb}_2\text{O}_5$ .<sup>5)</sup>

The surface areas of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  were 164, 126, and 42  $\text{m}^2 \text{g}^{-1}$  after the evacuation at 100, 300, and 500 °C, respectively.

**Acidic and Basic Character of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$ .** The acid strength of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  examined by the indicator adsorption method is mentioned first. After drying at 100 °C,  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  changed the color of benzylideneacetophenone ( $\text{p}K_a = -5.6$ ) indicator to its acidic color (yellow), but no color change of anthraquinone ( $\text{p}K_a = -8.2$ ) was observed. After heat treatment at 300 °C, all the indicators of  $\text{p}K_a \geq -8.2$  also changed their colors to those of the acidic forms. Thus,  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  which was heated at 100–300 °C has an acid strength of  $H_0 \leq -5.6$ . However, the strong acid sites disappeared and only an acid strength of  $H_0 \leq +3.3$  was observed by heating at 500 °C.

In order to obtain further information about the acidity of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$ , the infrared spectroscopic study of the adsorbed pyridine was examined. The results are shown in Fig. 2. Upon the adsorption of pyridine over  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  which had been evacuated at various temperatures, the bands at 1610, 1540, 1480, and 1440  $\text{cm}^{-1}$  were observed after degassing at 100–150 °C. The bands at 1610, 1480, and 1440  $\text{cm}^{-1}$  are due to co-ordinated pyridine and the band at 1540  $\text{cm}^{-1}$  is ascribed to pyridinium ion.<sup>6)</sup> Thus,  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  has both Lewis and Brønsted acid sites on the surface. The pyridinium ion band almost disappeared after degassing at 300 °C, but the Lewis acid bands still remained. The band intensity changes with evacuation temperature on  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  which had been preheated in a vacuum at different temperatures are shown in Fig. 3. The Brønsted acid band intensity was strongest on the sample evacuated at 100 °C and decreased with the increase of

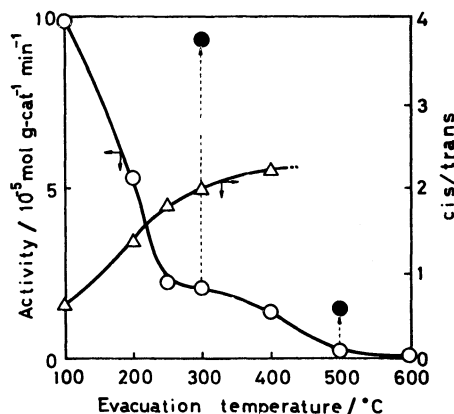


Fig. 5. Activity and selectivity of 1-butene isomerization. ●:  $\text{H}_2\text{O}$  added after pretreatment and evacuated at 100 °C.

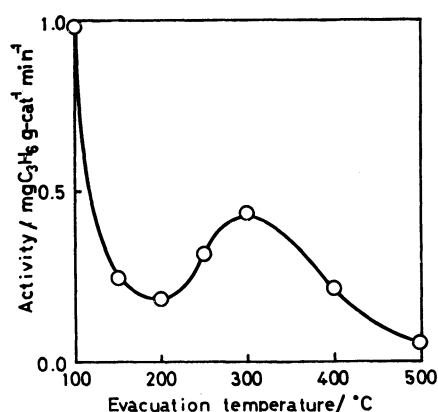


Fig. 6. Polymerization activity of propylene over  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$ .

pretreatment temperature. However, Lewis acid band intensity showed a maximum on the sample which had been evacuated at 300 °C. Upon preheating at 500 °C, both the acidic sites decreased remarkably.

The adsorption of  $\text{CO}_2$  on  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  was examined to obtain an information about surface basic property. The spectra are shown in Fig. 4. After the introduction of  $\text{CO}_2$  (2.7 kPa) on the sample which had been evacuated at 300 °C, no distinct change on the spectrum was observed. When the sample was contacted with  $\text{CO}_2$  for 15 h, a slight increase of the bands at 1600 and 1390  $\text{cm}^{-1}$  were noticed.

**Isomerization of 1-Butene.** The activity and selectivity changes of 1-butene isomerization with evacuation temperature are shown in Fig. 5. The  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  which was evacuated at 100 °C for 2 h showed a remarkable isomerization activity, the selectivity (the ratio of *cis*-2-butene to *trans*-2-butene) being less than unity. However, if the pretreatment temperature was increased to 200–250 °C, the activity decreased remarkably and the selectivity increased to about 2. In the range of evacuation temperature of 250–400 °C, the activity was not sensitive to the treatment temperature but diminished after the treatment at 500–600 °C. When  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  which had been evacuated at 300 °C was exposed to  $\text{H}_2\text{O}$  vapor at room temperature followed by

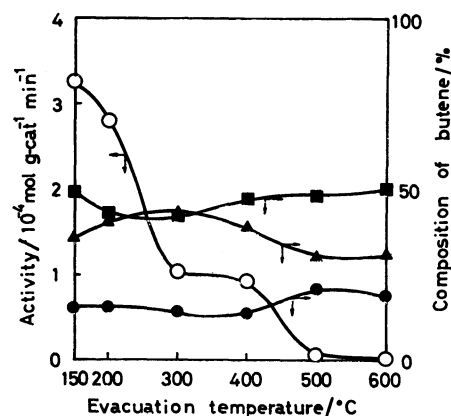


Fig. 7. Activity and selectivity changes of 2-butanol over  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  evacuated at various temperatures. ●: 1-Butene, ▲: *trans*-2-butene, ■: *cis*-2-butene

evacuation at 100 °C, almost the same activity as the catalyst originally evacuated at 100 °C was restored. On the other hand, after evacuation at 500 °C, the activity actually increased by the same treatment but the effect was far less compared to the case evacuated at 300 °C.

**Polymerization of Propylene.** The change of polymerization activity at 100 °C with evacuation temperature is shown in Fig. 6. The activity was highest on the sample evacuated at 100 °C and decreased remarkably after evacuation at 150–200 °C. However, upon evacuation at higher temperatures, the activity increased again and attained a maximum on treatment at 300 °C. After evacuation at the temperatures higher than 500 °C, the catalyst became almost inactive. The products of polymerization were not thoroughly analyzed due to the adsorption on the sample, but a considerable amount of butenes and pentenes along with the higher hydrocarbons desorbed at higher temperature (300 °C).

**Dehydration of 2-Butanol.** The changes of activity and selectivity of 2-butanol dehydration reaction with evacuation temperature are shown in Fig. 7. The activity gradually decreased with evacuation temperature. However, the activity was not changed by evacuation between 300–400 °C. The activity finally diminished on evacuation at 500–600 °C.

The formation of dehydrogenated product was not observed in the reaction at 150 °C over the whole catalysts. The ratio of formed *cis*- and *trans*-2-butenes was almost unity and the amount of 1-butene was less than 20% of the products over the catalysts evacuated at lower temperatures (150–300 °C), but the amount of 1-butene increased and that of *trans*-2-butene decreased after evacuation at 400–500 °C.

## Discussion

The surface of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  showed a considerable strong acidic character and rather weak basic property. After heat treatment at 100 °C, the strong acid sites of  $H_0 \leq -5.6$  were found to exist on the surface. Over the typical solid acid catalysts such as  $\text{SiO}_2\text{-Al}_2\text{O}_3$  and  $\text{SiO}_2\text{-TiO}_2$ , the strong acid sites appear only after heat treatment at high temperature ( $\approx 500$  °C)<sup>7)</sup> along with the

removal of surface water. The acid sites on those catalyst surfaces are thought to be the isolated OH groups as Brönsted acid sites and the exposed metal ions as Lewis acid sites both of which appear after rigorous heat treatment.<sup>7)</sup> However,  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  has acidic OH groups (Brönsted acid sites) as observed by IR experiment even after the mild heat treatment at 100 °C. Thus, the surface acidic property of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  pretreated at mild temperatures is very peculiar and interesting because the residual water might cover almost the whole surface after the treatment. Upon pretreatment at 300 °C,  $\text{H}_2\text{O}$  was almost removed from  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  as observed in DTA experiment, and Lewis acidity increased along with the decrease of Brönsted acidity. However, after treatment at 500 °C,  $\text{Nb}_2\text{O}_5$  became very inactive and the acidic property was very weak. This surface change is considered to be due to a phase transformation of amorphous  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  to T-T phase  $\text{Nb}_2\text{O}_5$ <sup>5)</sup> at around 500–600 °C as observed by DTA and XRD. The catalytic activity of  $\text{Nb}_2\text{O}_5$  was diminished by heat treatment at 500 °C or higher temperatures in the whole cases of 1-butene isomerization, propylene polymerization and 2-butanol dehydration reactions. In the case of 1-butene isomerization,  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  was very active on evacuation at 100 °C. The ratio of produced cis- and trans-isomers was around unity as observed in a typical case of acid-catalyzed reaction over  $\text{SiO}_2\text{--Al}_2\text{O}_3$ .<sup>8)</sup> Though the activity decreased drastically after the sample was evacuated at 300 °C, almost the same activity as the sample evacuated at 100 °C was restored only by the introduction of  $\text{H}_2\text{O}$  vapor followed by evacuation at 100 °C. This fact indicates that the isomerization is catalyzed mainly by Brönsted acid sites whose amount decreases with the increase of evacuation temperature as shown in Fig. 3. However, after evacuation at 500 °C, only a slight increase of activity was observed by the introduction of  $\text{H}_2\text{O}$  vapor. The decrease of surface area due to the phase transformation at around 500 °C might prevent the regeneration of Brönsted acid sites on the surface.

In the reaction of 2-butanol dehydration, a high activity was achieved by evacuation at 150–200 °C. The activity on the catalyst evacuated at 150 °C was almost comparable to that on  $\text{SiO}_2\text{--Al}_2\text{O}_3$  ( $3.7 \times 10^{-4}$  mol min<sup>-1</sup> g<sup>-1</sup> at 200 °C).<sup>9)</sup> Since the activity was reduced remarkably by evacuation at 300 °C, the activity would be also ascribed to Brönsted acidity, but Lewis acid sites might also act as active sites on evacuation at 300–400 °C. It is known that the selectivity of produced butenes from 2-butanol is very sensitive to the surface acidic and basic property.<sup>10)</sup> The oxide catalysts which have both acidic and basic sites such as  $\text{ThO}_2$  and  $\text{ZrO}_2$  produce 1-butene dominantly.<sup>11)</sup> However, over the strongly acidic catalysts such as  $\text{SiO}_2\text{--Al}_2\text{O}_3$  produce less amount of 1-butene than 2-butene.<sup>12)</sup> The  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  in this experiment is the latter case. It would be reasonable because the surface of  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  was mainly acidic and only very weak basic sites were observed in IR of  $\text{CO}_2$  adsorption or indicator adsorption.

The polymerization of propylene is known as a model

reaction catalyzed by Brönsted acid sites over  $\text{SiO}_2\text{--Al}_2\text{O}_3$  or other acid catalysts.<sup>13)</sup> In this work,  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  evacuated at 100 °C showed the highest activity for the polymerization, but the activity decreased remarkably when evacuated at 200–250 °C. In this case, it might be reasonable that the activity is ascribed to Brönsted acidity. However, the activity increased again on evacuation at 300–400 °C in contrast to the cases of 1-butene isomerization and dehydration of 2-butanol. This fact suggests the importance of Lewis acidity in the polymerization of propylene over  $\text{Nb}_2\text{O}_5$  evacuated at higher temperatures. It is known that niobium compounds such as niobium trichloride distearate and niobium tetrachloride butanoate can polymerize ethylene, propylene, and 1,3-butadiene.<sup>14)</sup> The promoting effect of niobium halide in the polymerization in Ziegler-Natta system is also known in the patent.<sup>15)</sup> Since the importance of niobium ion as an active site for the polymerization is apparent in those cases, the Lewis acid site is thought to be an active site even on the oxide of niobium. Thus, we conclude that the polymerization of propylene proceeds on Brönsted acid sites on  $\text{Nb}_2\text{O}_5 \cdot n\text{H}_2\text{O}$  pretreated at low temperatures ( $\approx 100$  °C), but Lewis acid sites become main active sites after treatment at higher temperatures.

In conclusion, niobium oxide treated at 100 °C is characterized as a very strong Brönsted acid and can be used as a potential catalyst for Brönsted acid-catalyzed reactions at mild conditions. It should be emphasized that niobium oxide exhibits the highest acid strength among all of the metal oxides pretreated at 100 °C.

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## References

- 1) R. Parthasarathy and J. G. Ciapetta, France Patent, No. 1555139 (1968); T. Shirasaki, K. Moriya, and I. Furuoya, Japan Patent, 76-143615 (1976); Y. Oda, K. Uchida, and T. Morimoto, Japan Patent, 73-49715 (1973); Y. Nanba, T. Suzuki, Y. Nakanishi, and Y. Okuda, Japan Patent, 75-39292 (1975).
- 2) J. F. McMahon, France Patent, No. 1500632 (1966); R. C. Hansford, U. S. Patent, No. 3480684 (1969); L. Bajars, U. S. Patent, No. 3291854 (1966); L. Bajars, U. S. Patent, No. 3308200 (1967); L. Bajars, U. S. Patent, No. 3308196 (1967); L. Bajars, U. S. Patent, No. 3308191 (1967).
- 3) K. Ohdan, H. Sasaya, K. Yoshida, and H. Ohtsuka, Japan Patent, No. 73-55870 (1973).
- 4) K. Tanabe, "Solid Acids and Bases," Kodansha, Tokyo, Academic Press, New York (1970).
- 5) M. L. Robinson, *J. Phys. Chem. Solids*, **29**, 2064 (1967).
- 6) E. P. Parry, *J. Catal.*, **2**, 371 (1963).
- 7) M. Itoh, H. Hattori, and K. Tanabe, *J. Catal.*, **35**, 225 (1974).
- 8) J. W. Hightower and W. K. Hall, *Chem. Eng. Prog., Symp. Ser.*, **63**, 122 (1967).
- 9) K. Tanabe, A. Kayo, and T. Yamaguchi, *J. Chem. Soc., Chem. Commun.*, **1981**, 602.
- 10) M. E. Winfield, *Catalysis*, **7**, 93 (1960).
- 11) A. J. Lundeen and R. V. Hoozer, *J. Org. Chem.*, **32**,

3386 (1967); T. Yamaguchi, H. Sasaki, and K. Tanabe, *Chem. Lett.*, **1973**, 1017.

12) A. J. Lundeen and R. V. Hoozer, *J. Am. Chem. Soc.*, **85**, 2180 (1963).

13) M. W. Tamele, *Discuss. Faraday Soc.*, **8**, 270 (1960).

14) J. E. Bwileigh and C. A. Ura-neck, U. S. Patent, No. 3640986 (1972).

15) K. Tashiro, M. Yokoyama, and S. Kitazume, Japan Patent, 74-15631 (1974).

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